

Optimisation of $Poly(\gamma$ -Glutamic Acid) Production by *Bacillus* velezensis NRRL B – 23189 in Liquid Fermentation with Molasses as the Carbon Source without Addition of Glutamic Acid

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Abstract – Poly (γ -glutamic acid), also known as γ -PGA, is an extracellular polymer produced by microbial fermentation. It is water-soluble, edible, biodegradable, non-toxic towards humans and the environment, and it has many available sites for drug conjugation and a powerful ability to solubilise hydrophobic molecules. This work reports the application of molasses, citric acid and ammonium sulphate in the fermentation by Bacillus velezensis NRRL-23189 to produce γ -PGA and the detection of molasses consumption without the use of glutamic acid as a nutrient. Different concentrations of molasses, citric acid and ammonium sulphate were studied. The fermentation was agitated at 200 rpm at 27°C for 72 h, with an initial pH of 6.5 (NaOH 2N and HCl 2N). Spectrophotometric analyses were used to measure concentrations of γ -PGA and the residual sugar from molasses (200g/l), citric acid (12.5g/l) and ammonium sulphate (8g/l) in a fermentation that also resulted in the maximum sugar consumption. **Copyright** © **2012 Praise Worthy Prize S.r.l. - All rights reserved**.

Keywords: Bacillus, Molasses, Poly (γ-Glutamic Acid), Fermentation, Biosynthesis, Nutritional Requirements

I. Introduction

Poly(γ -glutamic acid), known as γ -PGA, is a biodegradable anionic polymer that is water-soluble [1]-[5] and non-toxic to humans and the environment [2], [6], [7]. γ -PGA is polymerised via γ -amide linkages between α -amino and γ -carboxylic acid groups linking subunits of D- and L- glutamic acid [3]-[6], [8]-[10]. Ivánovics and co-workers discovered the compound in 1937 as a capsule polymer of *Bacillus anthracis* [1], [12]. Later, γ -PGA was identified in other *Bacillus spp*. as a fermentation product, for example in Bacillus subtilis IFO 3335 [1], Bacillus licheniformes, Bacillus megaterium and Bacillus amyloliquefaciens [12]-[13][14]. After reference [12] showed that γ -PGA was produced as a fermentation product in a culture broth by Bacillus subtillis, numerous studies were stimulated [10]. γ -PGA is secreted by the cell wall and forms the capsule during growth [15] and is also excreted into culture media [15], [16]. γ-PGA biosynthesis in bacteria is carried out in two steps. The first step is the synthesis of L- and D- glutamic acid, and in the second step, D- and L- glutamic acid units are joined together [17]. γ -PGA is mainly produced from citric acid and ammonium sulphate (Fig. 1).

It is presumed that L-glutamic acid is produced from citric acid through isocitric acid and α -ketoglutaric acid in the tricarboxylic acid cycle (TCA), and γ -PGA is polymerised from this glutamic acid.

A large amount of γ -PGA is thus produced from citric acid and ammonium sulphate [10].



Fig. 1. γ-poly(glutamic acid) (PGA) synthesis in *Bacillus subtilis* IFO3335: 1, glutamine: 2-oxoglutarate aminotransferase, 2, glutamine synthetase; 3, L-glutamic acid: pyruvic acid aminotransferase; 4, alanine racemase; 5, D-glutamic acid: pyruvic acid aminotransferase; 6, PGA polymerase; TCA, tricarboxylic acid [10]

 γ -PGA's characteristics enable its wide application as a biodegradable thickener, humectant, sustained release material and drug carrier in the food, cosmetic medical [1], [10], [18] and pharmaceutical industries [3]. γ -PGA and its derivatives can potentially be used as substitutes for petroleum-based hydrogels and thermoplastic polymers because γ -PGA is highly water-absorbent and biodegradable [19].

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 γ -PGA production by bacteria has diverse nutritional requirements [1], [10]. Some microorganisms require different carbon sources, others have unknown nitrogen sources and many of these do not require glutamic acid. Other bacteria grow only in the presence of glutamic acid [10] and some require biotin to produce γ -PGA [1], [10]. Reference [1] found that glutamic acid was not assimilated when added to the medium. The glutamic acid subunit in γ -PGA is produced from citric acid and ammonium sulphate. γ -PGA production is significantly induced by L-glutamate and the presence of L-glutamate results in the synthesis of highly elongated chains [20].

This paper reports the effect of molasses, citric acid and ammonium sulphate concentrations on γ -PGA production by *Bacillus velezensis* NRRL B – 23189 without the addition of glutamic acid to the fermentation medium. Molasses sugar consumption was also studied.

II. Materials and Methods

II.1. Bacterial Strain and Medium

Bacillus velezensis NRRL B – 23189 from the ARS Culture Collection (NRRL) was used in the study. BHI medium (brain heart infusion) with 20 g/l of bacteriological agar, both from Oxoid, was used for culture maintenance. Bacterial cells were incubated in agar slants at 32°C for 48 h and stored at 4 °C.

A medium reported by Bajaj and co-authors (2009) was modified for use in γ -PGA production as follows (g/l): K₂HPO₄, 1; MgSO₄.7H₂O, 0.5; CaCl₂.2H₂O, 0.2; MnSO₄.7H₂O, 0.05. The molasses, citric acid and ammonium sulphate concentrations used are shown in Table I. The initial pH was adjusted to 6.5 by using 6 N NaOH, 2 N NaOH and/or 2 N HCl. The medium was sterilised in an autoclave for 15 min at 121 °C.

II.2. Inoculum and Fermentation

The inoculum was produced as described below. A loopful of cells from a slant was collected and transferred to 50 ml of BHI medium in a 250-ml conical flask and incubated at 32 °C and 200 rpm for 12 h in a shaking incubator (TECNAL, mod. TE 421).

Fermentation was carried out in 250-ml Erlenmeyer flasks, each containing 45 ml of the sterile production medium. The medium was inoculated with 10 % (v/v) of a 12-h-old *Bacillus velezensis* NRRL 23189 culture containing approximately 2×10^{-3} g cells/ml BHI medium. The flasks were incubated for 72 h on a rotary shaker at 27 ± 2 °C and 200 rpm. Each fermentation assay was repeated twice. The samples were collected at the end of 72 h of fermentation for γ -PGA and residual sugar quantifications.

II.3. Surface-Response Methodology

The surface-response methodology (SRM) was used

to obtain a model for γ -PGA production and sugar consumption.

A Central Composite Design (CCD) was used to formulate a medium that provides optimal support for γ - PGA production by *Bacillus velezensis*.

The factorial planning had 4 central points and yielded a total of 18 treatments. The factors and levels studied are described in Table I.

TABLE I	
FACTORS AND LEVELS STUDIED IN THE CCD WITH 18 OBSERVATIONS	

Eastors	F	Factor level	*2
Factors	-1	0	+1
Molasses - 54 % TRS*1 (x1)	140.5	200	259.5
Citric Acid (x2)	5.06	12.5	19.94
Ammonium Sulfate (x3)	4	8	12

*1TRS: Total reducing sugars.

*² Components (g/l).

The results were analysed using Statistic 5.0 software. When several factors are involved, the model can be expressed as follows:

$$Y = bo + \sum_{i=1}^{4} bi \ xi + \sum_{i=1}^{4} bii \ xi2 \sum_{i \neq j=1} \sum bij \ xi \ xi$$
(1)

where *bo*, *bi*, *bii* and *bij* are the intercept term, linear, quadratic coefficient and interactive coefficient, respectively, and *xi* and *xj* are coded independent variables.

II.3.1. Determination of γ -PGA and Residual Sugar From Molasses

Cells were separated from the broth by centrifugation for 20 min at 2300 g (Excelsa Baby II, FANEM, model 206-R). The supernatant was collected for determination of the γ -PGA and residual sugar concentrations.

The γ -PGA concentrations were determined according to the method reported by [21].

The residual sugar concentration was monitored turbidometrically at 540 nm according to the method reported by [22].

III. Results and Discussion

Table II shows γ -PGA production and sugar consumption.

Reference [2] and reference [1] showed that when the glycerol concentration or other carbon source was increased in fermentation broth, a large amount of γ - PGA production occurred. When molasses was used as the carbon source, increased concentrations did not increase γ -PGA biosynthesis. When the concentration of molasses was 200 g/l or more, a decrease in γ -PGA production occurred.

An important observation is that sugar consumption was high when γ -PGA production was high.

	1-10	JAI KODUCTION AND S	UGAR CONSUMPTION			_
Treatments		Factors		$PCA(a 1^{-1})$	TDC* (a 1-1)	
Treatments	x1	x2	x3	$-\gamma$ -PGA (g.1)	1K3* (g.1)	
1	-1(140.5)	-1(5.06)	-1(4)	2.284	35.205	
2	+1(259.5)	-1(5.06)	-1(4)	2.036	86.804	
3	-1(140.5)	+1(19.94)	-1(4)	4.444	27.094	
4	+1(259.5)	+1(19.94)	-1(4)	3.700	74.034	
5	-1(140.5)	-1(5.06)	+1(12)	2.319	30.200	
6	+1(259.5)	-1(5.06)	+1(12)	2.674	84.215	
7	-1(140.5)	+1(19.94)	+1(12)	4.550	36.413	
8	+1(259.5)	+1(19.94)	+1(12)	2.355	109.929	
9	-1.68(100)	0(12.5)	0(8)	3.736	14.496	
10	+1.68(300)	0(12.5)	0(8)	3.665	102.853	
11	0(200)	-1.68(0)	0(8)	3.063	47.630	
12	0(200)	+1.68(25)	0(8)	3.559	35.205	
13	0(200)	0(12.5)	-1.68(1.28)	4.338	29.683	
14	0(200)	0(12.5)	+1.68(14.72)	3.700	39.347	
15	0(200)	0(12.5)	0(8)	4.904	27.612	
16	0(200)	0(12.5)	0(8)	4.621	22.780	
17	0(200)	0(12.5)	0(8)	5.117	26.231	
18	0(200)	0(12.5)	0(8)	4.630	24.160	

TABLE II

*TRS: Total reducing sugars

TABLE III REGRESSION COEFFICIENTS OF CCD

	Regression Coefficients	Pure error			95 % Confidence interval	
Factor			t	р	Lower bound	Upper bound
Interceptation/Mean	4,845	0,316	15,353	0,000	4.117	5.573
Molasses (L*)	-0,216	0,171	-1,263	0,242	-0.611	0.178
Molasses (Q*)	-0,517	0,178	-2,908	0,020	-0.927	-0.107
Citric Acid (L)	0,481	0,171	2,813	0,023	0.087	0.876
Citric Acid (Q)	-0,655	0,178	-3,683	0,006	-1.064	-0.243
Ammonium Sulfate (L)	-0,120	0,171	-0,702	0,503	-0.514	0.274
Ammonium Sulfate (Q)	-0,404	0,1780	-2,275	0,053	-0.814	0.006
Molasses X Citric Acid	-0,381	0,223	-1,704	0,127	-0.896	0.135
Molasses X Ammonium Sulfate	-0,106	0,223	-0,474	0,648	-0.621	0.409
Citric Acid X Ammonium Sulfate	-0,239	0,223	-1,069	0,316	-0.754	0.276

*L = linear, Q = quadratic

The maximum γ -PGA production occurred in treatments 15, 16, 17 and 18. These treatments are central points at level 0, and correspond to 200 g/l molasses, 12.5 g/l citric acid and 8 g/l ammonium sulphate. Assays 3, 7 and 13 showed similar γ -PGA production but with different media compositions.

The minimum γ -PGA production occurred in trials with low molasses, citric acid and/or ammonium sulphate concentrations or in which all the concentrations were maximum (Figs. 2, 4, 6). An equation for γ -PGA production was developed based on a regression analysis of the experimental data:

$$Y = 4.845 - 0.216x1 - 0.517x1^{2} + 0.481x2 + -0.655x2^{2} - 0.120x3 - 0.404x3^{2} - 0.381x1 \cdot x2 + -0.106x1 \cdot x3 - 0.239x2 \cdot x3$$
 (2)

Eqn. (2) produced results that were highly significant (P < 0.05), as shown in Table III, and the value of the coefficient of determination (R²=0.810) was satisfactory. The factor effect that more influences the γ -PGA production was citric acid (p < 0.05). In general, all effects present little influenced on the γ -PGA production.

An equation for sugar consumption was developed based on a regression analysis of the experimental data:

$$Y = 24.497 + 27.434x1 + 14.960x12 + +8.858x22+6.418x32$$
(3)

Eq. (3) produced results that were highly significant (P < 0.10) (Table IV), and the value of the coefficient of determination ($R^2 = 0.897$) was satisfactory.

TABLE IV Regression Coefficients Of The CCD						
Factor Regression Coefficients	Regression	Pure	t	р	90 % Confidence interval	
	error			Lower bound	Upper bound	
Interceptation/	24.498	5.471	4.478	0.0006	14.809	34.186
Mean						
Molasses (L*)	27.434	2.965	9.252	0.0000	22.183	32.686
Molasses (Q*)	14.960	3.081	4.855	0.0003	9.503	20.416
Citric Acid (Q)	8.858	3.081	2.875	0.0130	3.402	14.315
Ammonium Sulfate (O)	6.418	3.081	2.083	0.0576	0.962	11.874

*L = linear, Q = quadratic.

International Review of Chemical Engineering, Vol. 4, N. 6 Special Section on 4th CEAM 2012 - Virtual Forum All factors shown in Table IV influenced sugar consumption (p < 0.10). The effects of molasses, citric acid and ammonium sulphate on γ -PGA production and residual sugar concentrations are shown in Figures 2-7, respectively. The non-explicit variables were fixed at the central point (level 0) for the surface construction.

Maximum γ -PGA productivity was obtained using 4 different formulations of the initial concentrations of molasses, citric acid and ammonium sulphate. The figures show that maximum γ -PGA production occurred when the initial concentrations of molasses, citric acid and ammonium sulphate were between 140 and 200 g/l, 12.5 and 19.94 g/l, 4 and 12 g/L, respectively.



Fig. 2. Surface-response plot for the effect of molasses (x1) and citric acid (x2) on γ -PGA production

Residual Sugar (g/l)

160 140 Residual Sugar (gl) 120 100 80 60 40 2C 0 ഷ് ъ . . . Offic: de la com S 700

Fig. 3. Surface-response plot for the effect of molasses (x1) and citric acid (x2) on sugar consumption. The molasses contained 54% total reducing sugar



Fig. 4. Surface-response plot for the effect of molasses (x1) and ammonium sulfate (x3) on γ -PGA production



Fig. 5. Surface-response plot for the effect of molasses (x1) and ammonium sulfate (x3) on sugar consumption. The molasses contained 54% total reducing sugar

The maximum γ -PGA production was obtained when sugar consumption was at his maximum.

To choose the best result, assays 3, 7, 13 and 15 were duplicated. The results for γ -PGA production were analysed using the Tukey test 5% with Statistic 5.0 software. The results are shown in Table V.

TABLE V
Γ-PGA PRODUCTION BY BACILLUS VELEZENSIS NRRL B - 23189,
AT 27 °C FOR 72 H, INITIAL PH 6.5 AND 200 RPM

Treatments	γ -PGA (g.L ⁻¹)
3	$4,249 \pm 0,351^{a}$
7	$4,391 \pm 0,050^{a}$
13	$4,338 \pm 0,351^{a}$
15	4.798 ± 0.200^{a}

Matching letters indicate samples that did not differ statistically, and different letters indicate samples that differed at the 95 % confidence level

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Fig. 6. Surface-response plot for the effect of citric acid (x2) and ammonium sulfate (x3) on γ -PGA production



Fig. 7. Surface-response plot for the effect of citric acid (x2) and ammonium sulfate (x3) on sugar consumption. The molasses contained 54 % total reducing sugar

These experiments show that the amounts of molasses, citric acid and ammonium sulphate in the culture medium are important determinants for γ -PGA productivity by *Bacillus velezensis* NRRL 23189.

Increased concentrations of the carbon source increased the γ -PGA production only at the beginning of the fermentation, contrary to the observations of some references [2] and [16]. At concentrations of molasses, citric acid and ammonium sulphate above 200, 19.94 and 12 g/l, respectively, there was no increase in γ -PGA production. Several bacterial strains have been recently studied for γ -PGA production. Reference [21] reported a maximum productivity of 10.4 g/l using *Bacillus subtilis* BL53 cultivated at 37°C for 96 h. Reference [11]

reported a maximum productivity of 46.4 g/l using *Bacillus subtilis* ZJU-7 cultivated at 37 °C for 48 h. In other reported work [23], γ -PGA was produced using *Bacillus licheniformis* NCIM 2324 cultivated at 37°C for 96 h with maximum productivity of 26.12 g/l. *Bacillus velezensis* NRRL 23189 produces γ -PGA in media without glutamic acid, which is an advantage when compared with other *Bacillus* strains. This fact is important for industrial cost reduction because glutamic acid is a fermentation product, and the cost of molasses is cheaper than that of the purified sugars.

IV. Conclusion

Molasses, citric acid and ammonium sulphate in a fermentation medium without glutamic acid yielded γ - PGA production in batch fermentations using *Bacillus velezensis* NRRL 23189. A maximum γ -PGA concentration of approximately 4.8 g/l was achieved with 4 different formulations of the fermentation medium that also showed maximum sugar consumption. The production of γ -PGA without glutamic acid in the culture medium is advantageous.

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References

- A. Goto, M. Kunioka, Biosynthesis and hydrolysis of poly(γglutamic acid) from *Bacillus subtilis* IFO3335, *Biosci. Biotech. Biochem.* 56 (1992) 1031-1035.
- [2] R. Richard, A. Margaritis, Optimization of cell growth and poly(glutamic acid) production in batch fermentation by *Bacillus* subtilis, Biotechnology Letters 25 (2003) 465-468.
- [3] F. Shi, Z. Xu, P. Cen, Microbial production of natural poly amino acid, Sci China Ser B-Chem, 50 (2007) 291-303.
- [4] F. Shi, Z. Xu, P. Cen, Efficient production of poly-γ-glutamic acid by Bacillus subtilis ZJU-7, Applied Biochemistry and Biotechnology, 133 (2006) 271-281.
- [5] F. Shi, Z. Xu, P. Cen, Optimization of γ-polyglutamic acid production by *Bacillus subtilis* ZJU-7 using a surface-response methodology, *Biotechnology and Bioprocess Engineering*, 11 (2006) 251-257.
- [6] I. L. Shih, Y. T. Van, The production of poly-(γ-glutamic acid) from microorganisms and its various applications, *Bioresource Technology*, 79 (2001) 207-225.
- [7] S. H. Yoon, J. H. Do, S. Y. Lee, H. N. Chang, Production of polyγ-glutamic acid by fed-batch culture of *Bacillus licheniformis*, *Biotechnology Letters*, 22, (2000) 585-588.
- [8] M. Ashiuchi, H. Misono, Biochemistry and molecular genetics of poly-γ-glutamate synthesis, *Appl. Microbiol. Biotechnol.* 59 (2002) 9-14.
- [9] A. C. Chibnall, M. W. Ress, F. M. Richards, Structure of the polyglutamic acid from *Bacillus subtili*, *Bioch.* 68 (1958) 129-135.
- [10] M. Kunioka, Biosynthesis and chemical reactions of poly(amino acid)s from microorganisms, *Appl. Microbiol. Biotechnol.*, 47 (1997) 469-475.
- [11] J. Chen, F. Shi, B. Zhang, F. Zhu, W. Cao, Z. Xu, G. Xu, P. Cen, Effects of cultivation conditions on the production of γ-PGA with Bacillus subtilis ZJU-7, Appl. Biochem. Biotechnol. (2010) 370-

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International Review of Chemical Engineering, Vol. 4, N. 6 Special Section on 4th CEAM 2012 - Virtual Forum 377.

- [12] M. Bovarnick, The formation of extracellular d(-)-glutamic acid polypeptide by *Bacillus subtilis*, J. Biol. Chem. 145 (1942) 415-424.
- [13] M. Kambourova, M. Tangney, F. G. Priest, Regulation of polyglutamic acid synthesis by glutamate in *Bacillus licheniformis* and *Bacillus subtilis*, *Applied and Environmental Microbiology*, 67 (2001) 1004-1007.
- [14] C. B. Thorne, C. G. Leonard, Isolation of D- and L-glutamyl polypeptides from culture filtrates of *Bacillus subtilis*, J. Biol. Chem., 233 (1958) 1109-1112.
- [15] J. H. Do, H. N. Chang, S. Y. Lee, Efficient recovery of γ-poly (glutamic acid) from highly viscous culture broth, *Biotechnology* and *Bioengineering*, 76 (2001) 219-223.
- [16] M. Kunioka, A. Goto, Biosynthesis of poly(γ-glutamic acid) from L-glutamic acid, citric acid, and ammonium sulphate in *Bacillus* subtilis IFO3335, Appl. Microbiol. Biotechnol. 40 (1994) 867-872.
- [17] I. B. Bajaj, R. S. Singhal, Enhanced production of poly (γglutamic acid) from *Bacillus licheniformis* NCIM 2324 by using metabolic precursors, *Appl. Biochem. Biotechnol.* 159 (2009) 133-141.
- [18] A. Hoppensack, F. B. Oppermann-sanio, A. Steinbüchel, Conversion of the nitrogen content in liquid manure into biomass and polyglutamic acid by a newly isotated strain of *Bacillus licheniformis, FEMS Microbiology Letters* 218 (2003) 39-45.
- [19] H. J. Choi, M. Kunioka, Preparation conditions and swelling equilibria of hydrogel prepared by γ-irradiation from microbial poly(γ-glutamic acid), *Radiat. Phys. Chem.* 46 (1995) 175-179.
- [20] M. Ashiuchi, T. Kamei, D. H. Baek, S. Y. Shin, M. H. Sung, K. Soda, T. Yagi, H. Misono, Isolation of *Bacillus subtilis* (*chungkookjang*), a poly-γ-glutamate producer with high genetic competence, *Appl. Microbiol. Biotechnol.* 57 (2001) 764-769.
- [21] S. B. Silva, Produção e otimização de processo de obtenção de ácido γ-poliglutâmico através do cultivo de *Bacillus subtilis BL53*, PhD. Teses, Dept. Chemistry Engineering, Federal University of Rio Grande do Sul, Porto Alegre, RGS, 2010.
- [22] M. Somogy, Determination of blood sugar, Journal of Biological Chemistry (1945) 160-169.
- [23] I. B. Bajaj, S. S. Lele, R. S. Singhal, Enhanced production of poly(γ-glutamic acid) from Bacillus licheniformis NCIM2324 in solid state fermentation, *Journal of Industrial Microbiology and Biotechnology* 35 (2008) 1581-1586.

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